

# MANIPAL INSTITUTE OF TECHNOLOGY MANIPAL UNIVERSITY

#### I SEMESTER B.E DEGREE EXAMINATION NOVEMBER 2008



## SUBJECT: ENGG. CHEMISTRY.(CHM 101/102)

Scheme of Valuation

Time: 3 Hrs]			[Max. Marks: 50	
Note:	Answer any <b>FIVE</b> full questions			
1.	a) Give reason			
	i) $E = E^{0} - 0.0592 \log [Cl^{-}]$ Explanation ii) Two reasons1 M	a	½M	
	b) i) Defination1M Derivation of Mn a ii) One major difference with an example		-2M	
	c) i) Diagram $\frac{1}{2}$ M Conditions like Temp, Pressure Process1M Merits (any two) $\frac{1}{2}$ N ii) Calculation of G.C.V L = (W+w)(t <sub>2</sub> -t <sub>1</sub> )/x	-	1M	
	= (1458 + 456) ( 19.2-13,25)/0.945			
	$= 12.051 \text{ k cal g}^{-1}$		$\frac{1}{2}M$	
	LCV = 12051 - 8x0.09x586 = 11.629 k cal g <sup>-1</sup>		½M	

- 2. a) Give reason
  - i) The secondary reaction taking place in a dry cell is not a electrochemical reaction. It is the conversion of Zn into diammine Zn (II) chloride. So it do not contribute towards the overall

$$NH_4+(aq) + OH^{-}(aq) \rightarrow NH_3(g) + H_2O(l)$$
  
 $Zn^{2+}(aq)+2NH_3(s)+2Cl-\rightarrow [Zn(NH_3)_2Cl_2]$ 
1M

- ii) Due to overcharging electrolysis of water will take place which results in the accumulation of hydrogen and oxygen leading to explosion of the cell. If kept in a partially discharged condition sulphatation will take place.
- b) i)Explanation of function of anodic inhibitor with with an example 1M Explanation of functions of 2 types of cathodic inhibitor with an example each

2M

1 M

#### c) i) Definition of electroless plating

 $\frac{1}{2}M$ 

The catalytic metals such as Ni, Co, Steel, Pd etc., do not require any surface preparation before electro less plating on them. Non catalytic metals such as Cu, brass, Ag etc., need activation. This can be done by dipping in palladium chloride solution. Non conductors like glass, plastics, etc., are first activated in a solution of SnCl<sub>2</sub> and HCl. After rinsing its immersed in a solution of PdCl<sub>2</sub> and HCl. This treatment yields a thin layer of Pd on the treated surface.

 $1\frac{1}{2}$  M

HO—C—
$$(CH_2)_4$$
—C—OH +  $H_2N$ — $(CH_2)_6$ —NH<sub>2</sub> —  $H_3N$ — $(CH_2)_6$ —NH<sub>3</sub> adipic acid hexamethylene diamine heat,  $-H_2O$ 

O—C— $(CH_2)_4$ —C—NH— $(CH_2)_6$ —NH— $(CH_2)_6$ —NH

- (i) It is used as a plastic as well as fibre.
- (ii) This is used to produce tyre cord.
- (iii) It is used to make mono filaments and roaps.
- (iv)Nylon 6,6 is used to manufacture articles like brushes and bristles.

### Preparation of SBR

$$\begin{array}{c} H_2C = CH \\ \\ n \times \left[ H_2C = CH - CH = CH_2 \right] + n \end{array} \longrightarrow \underbrace{ \left[ H_2C - CH = CH - CH_2 \right]_X H_2C - CH}_{n}$$

#### **Uses:**

Mainly used for the manufacture of motor tyres.

Other uses of this elastomer are floor tiles, shoe soles, gaskets, foot-wear components, wire and cable insulations, carpet backing, adhesives, tank-lining, etc.,

- 3. a) Give reason:
  - i) Mentioning 2 types of cathodic reactions in aerated acid soulutions ½M Equations ½M
  - ii) Reason with proper explanation regarding passivating potential 1M
  - b) i) Development of electrode potential in a glass electrode:

The glass is a partially hydrated aluminosilicate containing sodium or calcium ions. The hydration of a pH sensitive glass membrane involves an ion-exchange reaction between singly charged cations in the interstices of the glass lattice and protons from the solution. The ion-exchange reaction can be written as

$$H^+$$
 +  $Na^+$  <====>  $Na^+$  +  $H^+$   
Solution glass solution glass  $\frac{1}{2}M$ 

Explanation for development of potential ½M.

Development of electrode potential of glass electrode:

The overall potential of the glass electrode has three components.

The boundary potential <sub>b</sub>, which varies with the pH of the analyte solution. It is made up of two potentials, E<sub>1</sub> & E<sub>2</sub> which develop at the two surface of the glass membrane i.e. the potential developed at the inner glass surface & the potential developed at the outer glass surface.

$$E_b = E_1 - E_2$$
 \_\_\_\_\_(1)

Where E<sub>b</sub> is the boundary potential

 $E_1$  = potential developed at the interface between the exterior of the glass and the analyte solution

 $E_2$  = Potential developed at the interface between the internal solution and the interior of the glass. The boundary potential is related to the concentration of hydrogen ion in each of the solution by the Nernst-like equation.

$$E_b = E_1 - E_2 = 0.0592 \log C_1 / C_2$$
 (2)

Where  $C_1$  = concentration of the analyte solution

 $C_2$  = concentration of the internal solution

For a glass pH electrode the hydrogen ion concentration of the internal solution is held constant. So eqn. (2) simplifies to

$$E_b = K + 0.0592 log C_1 \begin{subarray}{c} (3) \\ (K - 0.0592 pH \ where \ K = -0.0592 log C_2 \end{subarray}$$

The boundary potential is then a measure of the hydrogen ion concentration of the external solution.

- 2) The potential of the internal Ag/AgCl reference electrode. E Ag/AgCl.
- 3) A small unpredictable contribution called the asymmetry potential, E asym. The sources of the symmetry potential include the following.
  - (i) Differing conditions of strain in the two glass surfaces during manufacture
  - (ii) Mechanical abrasion on the on the outer surface during use
  - (iii) Chemical etching of the outer surface during use.

The asymmetry potential changes slowly with time. The glass electrode potential can be written in the equation form as

$$E_G = E_b + E_{Ag/AgCl} + E_{asym}$$
Substitution of eqn – (3) for  $E_b$ , gives
$$E_G = K + 0.0592 \log C_1 + E_{Ag/AgCl} + E \text{ asym}$$

 $= K - 0.0592 \log pH + E_{Ag/AgCl} + E$ asym

or  $E_G = E^o_G - 0.0592PpH$ where  $E_G^o = K + E_{Ag/AgCl} + E_{asym.}$ 

a combination of three constant terms = constant

 $\frac{1}{2}M$ 

 $\frac{1}{2}M$ 

ii) pH = 
$$E_{cell}$$
 /  $0.0592$ 

= 0.34/0.0592

= 5.74.

1M

c) i) Mechanism of petroleum knocking	1M
Prevention	1M

ii) Explanation for suspension polymerization  $1\frac{1}{2}M$ 

Any two differences between suspension and emulsion polymerization  $\frac{1}{2}M$ 

a) Reason: 4.

> i) Lower in C.V due to volatile matter  $\frac{1}{2}M$ Lower in C.V due to ash  $\frac{1}{2}M$

ii) Reason 1M

b) i) Cell Scheme:

Cd/Cd(OH)2,KOH,Ni(OH)2, Ni(OH)3/Ni  $\frac{1}{2}M$ 

Electrode reactions

Anode:

		$Cd(OH)_2(s)+2e- \rightarrow Cd(s) +2OH^-(aq)$	$^{1}/_{2}M$			
	Cathoo	de: $2Ni(OH)_{2(s)} + 2OH^{-}(aq) \rightarrow 2Ni(OH)_{3(s)} + 2e^{-}$	$^{1}/_{2}M$			
	Net:	$2Ni(OH)_{2(s)} + Cd(OH)_{2(s)} \rightarrow 2Ni(OH)_{3(s)} + Cd(s)$	$\frac{1}{2}M$			
	ii)	Any four requirements of the fuel cell Any two merits and demerits	1M 1M			
	ii) D	Explanation of caustic embrittlement with equations Definition of Tg Comparison of Tg values with structure 1	2M ½M ½M			
5.	i) Reas ii) Rea	e reason: son with proper explanation ason with suitable explanation $\Delta G = -nFE$ However all electrochemical reactions are accomp	1M 1M panied by			
	decrea	se in free energy of the system. Thus				
,		$-\Delta G = -nFE$ Hence e.m.f of the cell is positive	1M			
	$\Delta H = nF[T(\delta E/\delta T)_P - E]$					
	$= 2 \times 96500 (-2.952 \times 10^{-3} \times 298 - 0.7653)$					
	$= -2 \times 96500 \times 1.6444$					
		$= -317.48 \text{ k J K}^{-1}$ .	$^{1}/_{2}M$			
		$\Delta S = nF (\delta E / \delta T)_P$				
		$= -2 \times 96500 \times 2.952 \times 10^{-3}$				
	Chemic) i) D	= -0.5695 kJ ucture Property relationship with respect of plastic deformatical resistance Detailed procedure for ultimate analysis of coal of determination ydrogen with calculation steps.	2M			

# Percentage of nitrogen = $\frac{\text{Volume of acid used} \times \text{Normality of acid} \times 1.4}{\text{Weight of coal taken}}$

 $= 43.75 \times 0.1 \times 1.4 / 1.56$ 

= 3.92% 1M

Percentage of sulphur:

Wt. of BaSO<sub>4</sub> obtained  $\times$  32  $\times$  100 Wt. of coal taken  $\times$  233

 $= 0.1755 \times 32 \times 100 / 2.60 \times 233$ 

= 0.9270 %

6. a) Give reason

i) Explanation with equation

ii) Explanation for differential areation corrosion 1M

b) i) Explanation for the effect of two parameters on the rate of corrosion 1 mark each 2M

ii) Tacticity: Def ½M

Three different stuctural configuration of polypropylene 1 ½M

c) Origin of single electrode potential.

Explanation of the galvanization 2M

Reason ½M